

Physics 216

Lecture II - Ideal Fluids

- Equations
- Basic Concepts - especially Potential Flow
- Induced Mass, Quasi (Pseudo) Momentum

I.) Euler Equations / Ideal Fluids. "The Flow of Dry Water"

$$\begin{matrix} \vec{v}, \rho \\ \text{Volume } V \\ \text{density } \rho \end{matrix} \quad - \text{RDF}$$

- Mass conservation:

argue macroscopically
but really derive
from Boltzmann Eqs.

$$\frac{dM}{dt} = \frac{\partial}{\partial t} \int d^3x \rho(x,t) = - \int dS [v \rho]$$

$$= - \int d^3x \nabla \cdot (\rho v)$$

$$\boxed{\partial_t \rho + \nabla \cdot (\rho v) = 0} \quad \text{continuity}$$

$$\partial_t \rho + \nabla \cdot \underline{f} = 0$$

$$\underline{f} = \rho \underline{v}$$

* mass flux
density

- Momentum conservation:

$$\underline{F} = - \nabla P + \underline{f}$$

↓
fluid element ↓
pressure gradient ↓
Net force density
on element → body
force
 $(\frac{\Sigma x B}{c}$
on MHD)

o) Sir Isaac:

$$\rho \underline{a} = - \nabla P + \underline{f}$$

↑
acceleration

$$\underline{a} = \frac{d\underline{v}}{dt} \rightarrow \text{what does this mean (substantive derivative)}$$

here:

→ increment in \underline{v} ↓
displ.

$$\frac{d\underline{v}}{t} = \frac{\Delta \underline{v}}{\Delta t} dt + d\underline{r} \cdot \nabla \underline{v}$$

velocity
increment

↑
local
acceleration

particle moves/displaced.
in inhomogeneous
velocity field.

$$\frac{d\mathbf{v}}{dt} = \frac{\partial \mathbf{v}}{\partial t} + \frac{d\mathbf{r}}{dt} \cdot \nabla \mathbf{v}$$

$$= \frac{\partial \mathbf{v}}{\partial t} + \mathbf{v} \cdot \nabla \mathbf{v}$$

⇒

$$\rho \frac{d\mathbf{v}}{dt} = \rho \left(\frac{\partial \mathbf{v}}{\partial t} + \mathbf{v} \cdot \nabla \mathbf{v} \right) = -\nabla P + \mathbf{F}$$

Euler Eqn.

? Momentum Flux ?

$$\partial_t (\rho v_i) = - \frac{\partial}{\partial x_n} T_{ik}$$

i.e.

$$\partial_t (\rho v_i) = v \partial_t \rho + \rho \frac{\partial v}{\partial t}$$

momentum

$$\text{density} = -v \left(\rho \nabla \cdot \mathbf{v} \right) + \mathbf{v} \cdot \nabla \rho$$

$$+ \rho \left(-v \cdot \nabla v - \frac{\partial P}{\partial \rho} \right)$$

$$= - \left(\rho [v(\nabla \cdot v) + v \cdot \nabla v] \right) + v (\nabla \cdot \nabla \rho) - \nabla P$$

$$= -\nabla \cdot (\rho \underline{\underline{V}} \underline{\underline{V}} + \underline{\underline{I}} P)$$

↓ ↓
identity tensor
Reynolds
stress tensor

→ analogous to Maxwell stress tensor

so

$$\Pi_{ik} = \rho v_i v_k + \delta_{ik} P$$

and

$$\frac{\partial}{\partial t} \int d^3x \rho \underline{\underline{V}} = \frac{d}{dt} \underline{\underline{P}} = - \int d\underline{\Sigma} \cdot (\rho \underline{\underline{V}} \underline{\underline{V}} + \underline{\underline{I}} P)$$

$\Pi_{ik} dS_n$ ≡ momentum flux in i^{th} direction.

$$\boxed{\Pi_{ik} = \rho v_i v_k + \delta_{ik} P.}$$

defines
momentum
flux

- in N-S. Egn, viscous stress appears due momentum flux from collisions interacting with macroscopic flow gradients

→ Mass, Momentum and Energy!

In (ideal) fluid, no heat exchanged

between fluid elements \Rightarrow motion adiabatic - i.e. entropy conserved along trajectories

$$\frac{dS}{dt} = 0$$

$S \equiv$ entropy per mass.

$$\Rightarrow \boxed{\frac{\partial S}{\partial t} + \nabla \cdot \nabla S = 0}$$

{ adiabatic
equation for
fluid.

For energy Flux:

$$\Sigma = \rho \frac{v^2}{2} + \rho E$$

↳ internal
energy density
(i.e. thermal).

total energy density of fluid element

Now as with momentum, consider $\frac{d\Sigma}{dt}$,

① ②

$$\frac{d\Sigma}{dt} = \frac{\partial}{\partial t} \left(\rho \frac{v^2}{2} + \rho E \right)$$

$$\frac{\partial}{\partial t} \left(\frac{\rho u^2}{2} \right) = \frac{u^3}{2} \frac{\partial \rho}{\partial t} + \rho u \cdot \frac{\partial u}{\partial t}$$

$$= - \frac{u^3}{2} \underbrace{\nabla \cdot (\rho \underline{v})}_{\text{cont.}} - \underbrace{u \cdot \nabla P - \rho u \cdot (u \cdot \nabla u)}_{\text{Momentum balance.}}$$

$$u \cdot \nabla u = - \underline{v} \times \underline{\omega} + \frac{1}{2} \nabla (u^2)$$

$\underline{\omega} = \nabla \times \underline{v} \rightarrow \text{vorticity}$

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$$\begin{aligned} \rho u \cdot (u \cdot \nabla u) &= \rho u \cdot \left(-\underline{v} \times \underline{\omega} + \frac{1}{2} \nabla (u^2) \right) \\ &= \rho u \cdot \frac{1}{2} \nabla u^2 \end{aligned}$$

and

$$dW = dE + d(PV)$$

$$\text{enth=ly} = TdS + VdP$$

$$= TdS + \frac{dP}{\rho}$$

so

$$\nabla P = \rho \nabla u - \rho T \nabla S$$

Q.

thus, ①

$$\frac{\partial}{\partial t} \left(\frac{\rho v^2}{2} \right) = -\frac{v^2}{2} \nabla \cdot (\rho \underline{v}) - \rho \underline{v} \cdot \nabla \left(\frac{v^2}{2} + w \right) \\ + \rho T \underline{v} \cdot \underline{\nabla} \rho$$

For ② :

$$\frac{\partial}{\partial t} (\rho E) =$$

useful to transform using thermodynamic identity:

$$dE = dQ - \rho dV \\ = TdS - \rho dV$$

$$\text{but } V = 1/\rho$$

$$dV = -d\rho/\rho^2$$

$$dE = TdS + \frac{\rho}{\rho^2} d\rho$$

$$\therefore d(\rho E) = \rho dE + E d\rho$$

81

$$d(\rho\epsilon) = \left(\frac{\rho}{P} + \epsilon\right)d\rho + \rho T dS$$

$$\epsilon + \frac{P}{\rho} = \epsilon + PV = w$$

enthalpy

82

$$d(\rho\epsilon) = w d\rho + \rho T dS$$

$$\textcircled{2} \quad \frac{\partial}{\partial t} (\rho\epsilon) = w \frac{\partial P}{\partial t} + \rho T \frac{\partial S}{\partial t}$$

$$= -w \nabla \cdot (\rho V) - \rho T V \cdot \nabla S$$

So, combining \textcircled{1}, \textcircled{2}:

$$\begin{aligned} \frac{\partial}{\partial t} \left(\rho \frac{V^2}{2} + \rho \epsilon \right) &= -\frac{V^2}{2} \nabla \cdot (\rho V) - \rho V \cdot \nabla \left(\frac{V^2}{2} \right. \\ &\quad \left. + w \right) - w \nabla \cdot (\rho V) \\ &\quad - \rho T \cancel{V \cdot \nabla S} + \cancel{\rho T V \cdot \nabla S} \\ &= -\left(\frac{V^2}{2} + w \right) \nabla \cdot (\rho V) - \rho V \cdot \nabla \left(\frac{V^2}{2} + w \right) \\ &= -\nabla \cdot \left(\rho V \left(\frac{V^2}{2} + w \right) \right) \end{aligned}$$

Thus have:

$$\frac{\partial}{\partial t} \left(\frac{\rho v^2}{2} + \rho E \right) + \nabla \cdot (\rho v \left(\frac{v^2}{2} + w \right)) = 0$$

So

$$\frac{\partial}{\partial t} \int_V d^3x \left(\frac{\rho v^2}{2} + \rho E \right) = - \int \underline{ds} \cdot [\rho v \left(\frac{v^2}{2} + w \right)]$$

$\frac{\partial}{\partial t}$
change in energy
in volume V

\underline{ds}
energy flux
density
thru surface.

energy density flux

$$\underline{\Phi} = \rho v \left(\frac{v^2}{2} + w \right)$$

accompanied
 $\underline{T}_{ij}, \underline{D}$.

→ Meaning:

$$w = g + \underline{P}$$

(a) flux of KE and
internal energy

$$\begin{aligned} \int \underline{ds} \cdot \underline{\Phi} &= \int \underline{ds} \cdot \rho v \left(\frac{v^2}{2} + g \right) \text{ thru surface} \\ &+ \int \underline{ds} \underline{Q} v \frac{\rho}{\rho} \end{aligned}$$

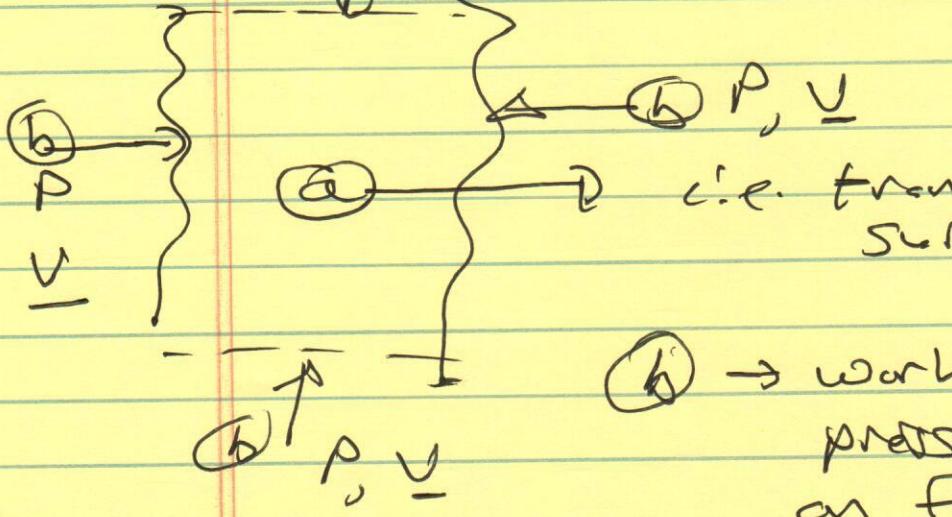
$$\textcircled{b} = \int \underline{dS} \cdot \underline{V} \cdot P$$

$\rightarrow P dV$ work done
by pressure
force on fluid
within surface.

$$= \int (\underline{V} \cdot \underline{dS}) P$$

$$dV/dt$$

$$\textcircled{a}, P, V$$



$\textcircled{b} \rightarrow$ work done by
pressure force
on fluid within S .

II.) Basic Concepts

Now convenient to note:

$$\begin{aligned} dE &= dQ - pdV \\ &= TdS - pdV \end{aligned}$$

$$W = E + PV$$

\rightarrow enthalpy as
Legendre transform
of entropy

then

$$dW = TdS + Vdp$$

$$= TdS + \underbrace{dp}_{P}$$

so, for isentropic motions ($dS = 0$),

$$\frac{dp}{\rho} = dW \quad \text{or} \quad \frac{\partial p}{\partial} = \underline{dW}$$

\rightarrow has advantage of RHS of
Euler Eqn. as perfect
derivative

$$\frac{\partial v}{\partial t} + v \cdot \nabla v = \frac{dv}{dt} = - \underline{dW}$$

Then, can immediately note:

$$\frac{d}{dt} \oint \underline{\mathbf{V}} \cdot d\underline{l} = 0$$

→ Circulation
conserved for
inviscid, isentropic
Fluid

i.e.

$$\frac{d}{dt} \oint \underline{\mathbf{V}} \cdot d\underline{l} = \oint \frac{d\underline{V}}{dt} \cdot d\underline{l}$$

\downarrow
Kelvin's Thm.

$$+ \oint \underline{\mathbf{V}} \cdot \frac{d\underline{l}}{dt}$$

$$= \oint \frac{d\underline{V}}{dt} \cdot d\underline{l} + \oint \underline{\mathbf{V}} \cdot \frac{d}{dt} d\underline{l}$$

$$= \oint (-\nabla w) \cdot d\underline{l} + \oint \underline{\mathbf{V}} \cdot d\underline{V}$$

$$= 0 + 0$$

i.e.

$$\oint \underline{\mathbf{V}} \cdot d\underline{l} = \text{const}$$

for closed
contour
in ideal,
isentropic
Fluid

13.

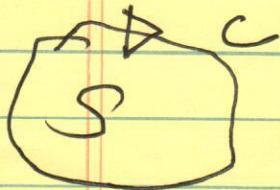
often:

Note: no use
 $\underline{D} \cdot \underline{V} = 0$

$$\Gamma = \oint \underline{V} \cdot d\underline{l} \rightarrow \text{conserved. (absolute)}$$

N.B.: obvious analogy in mechanics
 is Poincaré-Cartan invariant.

$$I_{PAC} = \oint \underline{P} \cdot d\underline{\Sigma} \quad \frac{d}{dt} I_{PAC} = 0$$



for Hamiltonian system.

Now, elementary vector calc. \Rightarrow
 normal to enclosed area.

$$\Gamma = \oint_C \underline{V} \cdot d\underline{l} = \int_A \underline{C} \cdot d\underline{\Sigma} \rightarrow \text{const.}$$

$$\underline{C} = \nabla \times \underline{V}$$

Vorticity

what is vorticity?

\rightarrow describes rotation of fluid element.

→ $\underline{\omega}$ is 2 \times effective local angular velocity of fluid.

i.e. $\underline{\sigma}_V = (\underline{\omega} \times \underline{r})/2$.

→ Vorticity is the non-trivial element of fluid dynamics beyond Bernoulli's Law and potential flow. Vorticity is central to all interesting topics.

Now,

$$\frac{\partial \underline{v}}{\partial t} + \underline{v} \cdot \nabla \underline{v} = -\nabla w$$

$$\begin{aligned} \underline{v} \cdot \nabla \underline{v} &= -\underline{v} \times (\underline{f} \times \underline{v}) + \nabla \frac{v^2}{2} \\ &= -\underline{v} \times \underline{\omega} + \nabla \frac{v^2}{2} \end{aligned}$$

\therefore Magnus Force

$$\frac{\partial \underline{v}}{\partial t} - \underline{v} \times \underline{\omega} = -\nabla \left(w + \frac{v^2}{2} \right)$$

then $\nabla \times$

\Rightarrow Ideal Vorticity (Induction) equation:

$$\left[\frac{\partial \underline{\omega}}{\partial t} = \nabla \times (\underline{v} \times \underline{\omega}) \right]$$

$$= -\underline{v} \cdot \nabla \underline{\omega} + \underline{\omega} \cdot \nabla \underline{v} - \underline{\omega} \nabla \cdot \underline{v}$$

$$\left[\frac{d \underline{\omega}}{dt} = \underline{\omega} \cdot \nabla \underline{v} - \underline{\omega} \nabla \cdot \underline{v} \right]$$

or with continuity:

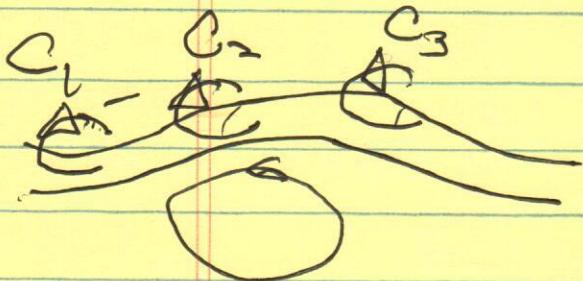
$$\left[\frac{d}{dt} \frac{\underline{\omega}}{\rho} = \frac{\underline{\omega}}{\rho} \cdot \nabla \underline{v} \right]$$

\rightarrow "frozen-in"

\rightarrow can derive Kelvin's Thm from induction equation

\rightarrow viscosity breaks circulation conservation.

III.) Potential Flow



excluded case
of separation/
o.

- Consider fluid streamlines

i.e. streamlines are lines along which fluid flows, i.e.

$$\frac{dx}{U_x} = \frac{dy}{U_y} = \frac{dz}{U_z}$$

then if $\omega = 0$ at any position streamline, Kelvin's thm $\Rightarrow \omega = 0$ everywhere on line

i.e. Easily seen by considering circulation around infinitesimal loops "pulled" along line. Thus if:

$$\oint \underline{U} \cdot d\underline{l} = \int \underline{\omega} \cdot d\underline{s} = 0, \text{ then } \begin{cases} \\ A_1 \end{cases}$$

$$\oint \underline{U} \cdot d\underline{l} = \int \underline{\omega} \cdot d\underline{s} = 0, \text{ all } C_n$$

- Flow with $\underline{\omega} = 0 = \nabla \times \underline{v}$ in all space
 \Rightarrow potential, irrotational flow.
- $\rightarrow \underline{\omega} \neq 0 \rightarrow$ vertical rotations/